

Sulfur Poisoning and Regeneration Behavior of Perovskite-Based NO Oxidation Catalysts

Merve Kurt¹ · Zafer Say¹ · Kerem Emre Ercan¹ · Evgeny I. Vovk^{1,2} ·
Chang Hwan Kim^{3,4} · Emrah Ozensoy¹

© Springer Science+Business Media New York 2016

Abstract SO_x uptake and release properties of LaMnO₃, Pd/LaMnO₃, LaCoO₃ and Pd/LaCoO₃ perovskites were investigated via in situ Fourier transform infrared (FTIR) spectroscopy, temperature programmed desorption and X-ray photoelectron spectroscopy. Sulfation of the perovskite leads to the formation of surface sulfite/sulfate and bulk-like sulfate species. Pd addition to LaMnO₃ and LaCoO₃ significantly increases the sulfur adsorption capacity. Pd/LaMnO₃ sample accumulates significantly more sulfur than LaMnO₃; however it can also release a larger fraction of the accumulated SO_x species in a reversible fashion at elevated temperatures in vacuum. This is not the case for Co-based materials, where thermal regeneration of bulk sulfates on poisoned LaCoO₃ and Pd/LaCoO₃ is extremely ineffective under similar conditions. However, in the presence of an external reducing agent such as H₂ (g), Pd/LaMnO₃ requires much lower temperature (873 K) for complete sulfur regeneration as compared to that of Pd/LaCoO₃ (973 K). Sequential CO and SO_x adsorption experiments performed via in situ FTIR indicate that in the presence of carbonyls and/or

carbonates, Pd adsorption sites may have a stronger affinity for SO_x as compared to that of the perovskite surface, particularly in the early stages of sulfur poisoning.

Keywords LaCoO₃ · LaMnO₃ · Pd · FTIR · DeNO_x · LNT

1 Introduction

Alleviating the air pollution associated with emissions from mobile applications is an important global problem. Particularly, hazardous gases such as CO, NO_x, SO_x and unburned hydrocarbons have been recently subject to increasingly more stringent emission regulations [1–3]. In order to meet such tough regulations, automobile industry is constantly searching for alternative technologies and novel catalytic materials. Lean burn engines have become very popular in recent years as they offer high fuel efficiencies and lower CO₂ emission. NO_x storage and reduction (NSR) catalytic technology is one of the most popular solutions for lean-NO_x aftertreatment applications [4–18]. NO oxidation/reduction ability and resilience against sulfur/phosphorous [13, 15, 19, 20] are among the most vital capabilities that are essential for such NO_x abatement (i.e. DeNO_x) applications. Precious group metals (PGM), particularly Pt, plays an important role in the DeNO_x oxidation/reduction pathways. However the use of Pt is economically unfavorable, as it significantly increases the overall cost of the catalytic DeNO_x system. Thus, search for Pt-free catalytic alternatives that can provide cost-effective and more competitive catalytic technologies has been carried out for a long time.

Along these lines, novel perovskite systems have been suggested as alternatives for catalytic NO oxidation and NO_x storage [21]. Lanthanum-based perovskite catalysts in

✉ Emrah Ozensoy
ozensoy@fen.bilkent.edu.tr

¹ Department of Chemistry, Bilkent University, 06800 Ankara, Turkey

² Boreskov Institute of Catalysis, 630090 Novosibirsk, Russian Federation

³ General Motors Global R&D Chemical Sciences and Materials Systems Lab, 30500, Mound Rd., Warren, MI 48090, USA

⁴ Present Address: Advanced Catalysts and Emission-control Research Lab, Powertrain Performance Development, R&D Division, 150, HyundaiYeonguso-ro, Hwaseong-si, Gyeonggi-do 445-706, Korea

the form of ABO_3 such as LaMnO_3 and LaCoO_3 are promising candidates for DeNO_x applications due to their inherently high oxidation capability, favorable NO_x conversion, low price and relatively simple synthesis procedures [21–24]. Perovskite catalysts, in general, have also been extensively studied in the literature where they have been demonstrated to be effective in catalytic oxidation, pollution abatement, catalytic hydrogenation/hydrogenolysis, photocatalysis, chemical sensors, electrolysis as well as in solid oxide fuel cell applications [25].

However, perovskite-based catalysts suffer from sulfur poisoning due to their basic surface sites [26, 27]. The interaction between various families of perovskites and SO_x species has been studied extensively in the literature. For instance, the interaction between LaCoO_3 and SO_2 was reported to yield $\text{La}_2(\text{SO}_4)_3$, $\text{La}_2(\text{SO}_3)_3$, $\text{La}_2\text{O}_2\text{SO}_4$, as well as CoO and Co_3O_4 species, where the latter species were suggested to form upon the destruction of the perovskite structure [28]. Annealing at higher temperatures was found to facilitate the removal of sulfates/sulfites, however complete regeneration of the LaCoO_3 perovskite structure was not feasible. Zhang et al. [29] also observed the destruction of the LaCoO_3 perovskite lattice via sulfur poisoning. Partial recovery of the LaCoO_3 structure was achieved by exposing the sample to a reducing atmosphere. Furthermore, substitution of different cations into the perovskite lattice and/or the addition of precious metals were found to increase the sulfur tolerance [21, 26, 28–30]. Recently, Wang et al. [31] investigated SO_2 tolerance and regeneration of $\text{LaCo}_{1-x}\text{Pt}_x\text{O}_3$ in NO_x storage and reduction processes. They compared their perovskite catalyst with a conventional $\text{Pt/Ba/Al}_2\text{O}_3$ NSR catalyst and reported that the perovskite had superior sulfur tolerance, regeneration capability and structural stability than the conventional NSR catalyst.

Recently, we have thoroughly investigated the synthesis, structural properties, NO_x oxidation/uptake and NO_x reduction behavior of LaMnO_3 , Pd/LaMnO_3 , LaCoO_3 and Pd/LaCoO_3 systems via transmission electron microscopy (TEM), X-ray diffraction (XRD), X-ray photoelectron spectroscopy (XPS), Raman spectroscopy, BET surface area analysis, in situ FTIR and TPD [32, 33]. In the current contribution, we focus on the molecular level investigation of the fundamental interactions that take place between SO_x species and LaMnO_3 , Pd/LaMnO_3 , LaCoO_3 and Pd/LaCoO_3 catalyst surfaces. Generation, thermal evolution, reduction and release of S-related surface and bulk-like functional groups as a function of temperature in vacuum as well as in the presence of an external reducing agent were systematically monitored by means of in situ FTIR and TPD. Along these lines, the nature of the sulfur adsorption sites on these perovskite systems and the effect

of sulfur poisoning on NO_x adsorption as well as catalytic regeneration behavior are discussed.

2 Experimental

2.1 Catalyst Preparation

LaMnO_3 and LaCoO_3 were prepared by using the citrate route [32]. For further details regarding the synthesis and structural characterization, the reader is referred to the discussion provided elsewhere [33]. Palladium supported perovskite materials was synthesized via conventional wetness impregnation method utilizing palladium nitrate along with LaCoO_3 or LaMnO_3 , where the perovskite materials were originally calcined at 973 K for 5 h in air. The nominal Pd loading was 1.5 wt% Pd in all of the synthesized catalysts. After the Pd loading, catalysts were further calcined at 773 K for 5 h in air.

2.2 Instrumentation

FTIR spectroscopic measurements were carried out in transmission mode in a batch-type catalytic reactor [9] coupled to an FTIR spectrometer (Bruker Tensor 27) and a quadrupole mass spectrometer (QMS, Stanford Research Systems, RGA 200). All FTIR spectra were acquired at 323 K. Prior to each experiment, materials were activated/cleaned using 2.0 Torr NO_2 gas at room temperature followed by heating at 973 K for 5 min under vacuum. NO_2 was prepared by the reaction of NO (99.9 % purity, Air Products) with O_2 (99.999 % purity, Linde AG) and further purified by subsequent freeze–pump–thaw cycles.

Poisoning experiments were carried out by exposing the sample surfaces to 2.0 Torr $\text{SO}_2 + \text{O}_2$ gas mixture ($\text{SO}_2:\text{O}_2 = 1:10$) at 300 K (SO_2 purity >99 %, Air Products). Then, samples were annealed to 323, 373, 473, 573, or 673 K and kept at these given temperatures for 15 min in the presence of the gas mixture. Thermal regeneration of the sulfur-poisoned perovskite catalysts was performed via annealing (heating rate = 12 K min^{-1}) at temperatures within 473–1073 K, where the samples were kept at chosen temperatures for 10 min in vacuum. Desulfation/reduction experiments with H_2 (99.995 % purity, Linde AG) were carried out by exposing the pre-sulfated samples (using the sulfation protocol given above) to 2.0 Torr of H_2 at 300 K followed by heating at various temperatures (i.e. 673–873 K for LaMnO_3 , and 673–973 K for LaCoO_3) in the presence of H_2 for 15 min. For the sequential SO_x and CO adsorption experiments, material surfaces were initially saturated with 50.0 Torr of CO (g) (99.995 % purity, Air Products) for 1 h at 323 K followed by evacuation at

$\sim 10^{-3}$ Torr. Next, these CO pre-adsorbed surfaces were exposed to 2.0 Torr SO_x mixture ($\text{SO}_2:\text{O}_2 = 1:10$) at 323 K.

SO_x TPD experiments were performed by initially exposing the materials with 2 Torr SO_x mixture ($\text{SO}_2:\text{O}_2 = 1:10$) at 673 K for 30 min followed by evacuating the reactor until the pressure reached 10^{-3} Torr. Then, materials were heated to 1173 K with a linear heating rate of 12 K min^{-1} in vacuum. $m/z = 32$ [corresponding to O_2 and S desorption where the latter is due to the impact ionization-induced fragmentation of desorbed SO_2 (g) in QMS], $m/z = 64$ [corresponding to SO_2 (g) desorption] and $m/z = 34$ [corresponding to H_2S (g) desorption] channels were monitored by QMS.

Ex-situ XPS analysis was performed using a SPECS photoelectron spectrometer equipped with a monochromatic Al $K\alpha$ X-ray source (1486.74 eV, 200 W) and a PHOIBOS-100 hemispherical energy analyzer with a MCD5 detector. Prior to the XPS analysis of the sulfur poisoned catalysts, catalyst surfaces were exposed to 10.0 Torr of $\text{SO}_2 + \text{O}_2$ gas mixture ($\text{SO}_2:\text{O}_2 = 1:10$) and annealed at 673 K for 30 min in the presence of the gas mixture.

3 Results and Discussion

3.1 Material Characterization

The detailed characterization of perovskite materials via XRD, TEM, BET, XPS, and Raman Spectroscopy was previously reported in one of our former publications [33]. XRD patterns of these materials revealed only perovskite phases with a major diffraction signal at 32.56° for LaMnO_3 and 32.84° , 33.21° for LaCoO_3 . Pd or PdO_x were not detected in the XRD measurements, however, TEM and XPS investigation clearly verified the presence of PdO/PdO_x particles with an average particle size of ca. 4 nm. The relative surface atomic ratio of perovskite samples determined by XPS measurements showed that the surface of these materials were enriched with lanthanum; most probably due to the presence of $\text{La}_2(\text{CO}_3)_3$, $\text{La}(\text{OH})_3$ and/or amorphous La_2O_3 domains.

3.2 FTIR Spectroscopic Analysis of SO_x Uptake/Release

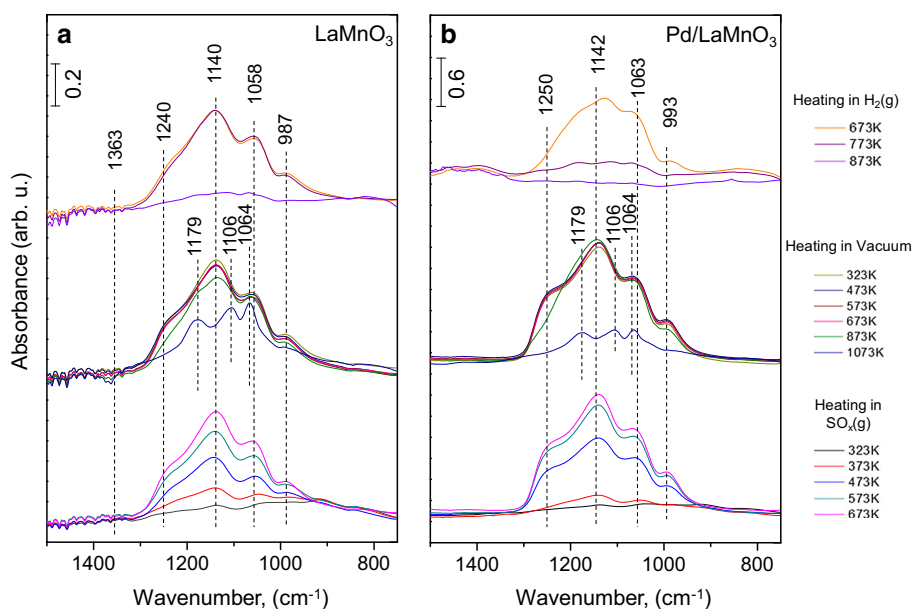
SO_x uptake and release properties of LaMnO_3 and Pd/LaMnO_3 perovskite materials were investigated via in situ FTIR as shown in Fig. 1. Sulfation of LaMnO_3 and Pd/LaMnO_3 reveals FTIR spectra with similar line shapes (bottom set of spectra in Fig. 1). Four main vibrational features at ca. 1240, 1140, 1058, and 987 cm^{-1} are

observed. While two of the former features are assigned to bulk-like sulfates, the latter two are attributed to bidentate surface sulfate species [13, 15]. The minor feature at 912 cm^{-1} , which is observed at the initial stages of sulfation is assigned to sulfite-like species [29]. Thermal annealing of pre-sulfated surfaces to 1073 K revealed sharper features at 1179, 1106, 1064, and 990 cm^{-1} . The second quadruplet was previously associated with bulk or subsurface sulfates as these species showed higher resistance towards reduction by NH_3 [34].

Considering the difference in scale bars of Fig. 1a, b (i.e. 0.2 and 0.6; respectively), one can readily realize that sulfation of Pd/LaMnO_3 (Fig. 1b) leads to almost three times higher SO_x -related IR absorption intensities as compared to that of Pd-free counterpart (Fig. 1a). Although it is not that feasible to make an accurate quantitative comparison of adsorbed SO_x species solely based on integrated FTIR spectra (due to differences in IR absorption cross sections of dissimilar oscillators and vibrational intensity transfer processes between oscillators [35]), it can be qualitatively argued that the presence of Pd leads to an increase in the SO_x uptake. This argument is also strongly supported by the XPS data that is presented in the forthcoming sections. It is most likely that exposed Pd sites catalyze the SO_2 oxidation and facilitate the sulfate accumulation on the catalyst surface. This increase in sulfur adsorption can be also tentatively attributed to the modification in the oxygen mobility of the perovskite surface due to the partial substitution of Pd into the B-sites of the perovskite on the surface [26]. Thermal regeneration of sulfur species in vacuum (middle sets of spectra in Fig. 1) at 373–673 K does not reveal any significant changes in IR spectra of LaMnO_3 and Pd/LaMnO_3 . However, after annealing at 873 K, the IR features associated with surface sulfates (i.e. 1058/1063 and $987/993 \text{ cm}^{-1}$) start to diminish. Most of the surface sulfur species are removed after annealing at 1073 K (Fig. 1a, b) while bulk-like sulfate related features at 1179, 1106, 1064, and 990 cm^{-1} still persist to exist even after high temperature thermal regeneration in vacuum [29, 36]. IR absorption intensities of the bulk sulfates are almost identical for both materials after the thermal treatment at 1073 K (note the difference in y-axis scale bars in Fig. 1a, b) in spite of the fact that Pd/LaMnO_3 (Fig. 1b) initially adsorbs more SO_x than LaMnO_3 (Fig. 1).

S-poisoned materials were also reduced under H_2 atmosphere in the temperature range of 673–873 K as illustrated in the top most sets of spectra in Fig. 1. Sulfates formed on LaMnO_3 are resilient to reduction up to 773 K (Fig. 1a), however, most of the bulk and surface sulfates are removed after reduction at 873 K. On the other hand, the sulfates on Pd/LaMnO_3 are less stable under reducing conditions as shown in Fig. 1b. On the sulfated $\text{Pd}/$

Fig. 1 FTIR spectra related to SO_x uptake and release properties of **a** LaMnO_3 , and **b** Pd/LaMnO_3 . *Bottom* set of spectra in each *panel* were acquired after SO_x exposure (2.0 Torr, $\text{SO}_2:\text{O}_2 = 1:10$) at 323 K, followed by annealing at 373, 473, 573, and 673 K in the SO_x gas mixture for 15 min. *Middle* set of spectra in each *panel* were acquired by heating at 473, 573, 673, 873, and 1073 K for 15 min under vacuum and after SO_x gas mixture was evacuated. *Upper* set of spectra were acquired by heating at 673, 773, and 873 K under 2.0 Torr of H_2 (g) for 15 min after SO_x gas mixture was evacuated. All spectra were acquired at 323 K in vacuum



LaMnO_3 catalyst (Fig. 1b), sulfate vibrational features significantly diminish even at 773 K and are completely removed at 873 K in the presence of hydrogen, while for LaMnO_3 (Fig. 1a), a significant portion of sulfates continue to exist on the surface at 773 K in hydrogen. Enhancement of sulfate reduction via H_2 in the presence of Pd can be explained by the dissociative chemisorption of H_2 on Pd sites and H-spill-over onto the perovskite surface [37]. A similar effect was also reported in the literature for an

entirely different reaction where Pd/LaMnO_3 and Pd/LaCoO_3 were found to exhibit higher methane conversion after sulfur regeneration via H_2 [26].

Identical FTIR experiments were also performed for Co-based perovskite materials (Fig. 2). FTIR spectra acquired upon sulfation of LaCoO_3 and Pd/LaCoO_3 at various temperatures (i.e. bottom set of spectra) are very similar to that of the Mn-based materials (Fig. 1). Thus, similar types of SO_x species seem to be forming on both Mn and Co-

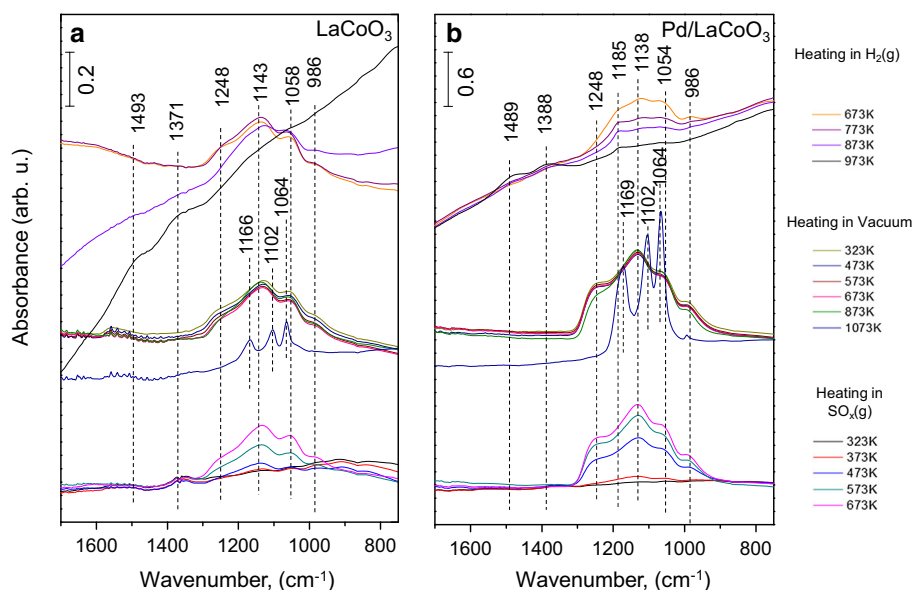


Fig. 2 FTIR spectra related to SO_x uptake and release properties of **a** LaCoO_3 , and **b** Pd/LaCoO_3 . *Bottom* set of spectra in each *panel* were acquired after SO_x exposure (2.0 Torr, $\text{SO}_2:\text{O}_2 = 1:10$) at 323 K, followed by annealing at 373, 473, 573, and 673 K in the SO_x gas mixture for 15 min. *Middle* set of spectra in each *panel* were

acquired by heating at 473, 573, 673, 873, and 1073 K for 15 min under vacuum and after SO_x gas mixture was evacuated. *Upper* set of spectra were acquired by heating at 673, 773, 873, and 973 K under 2.0 Torr of H_2 (g) for 15 min after SO_x gas mixture was evacuated. All spectra were acquired at 323 K in vacuum

based perovskites. Moreover, based on FTIR intensities (as well as the current XPS results that are discussed in the forthcoming sections) one can infer that LaMnO_3 (Fig. 1a) reveals a higher sulfur accumulation as compared to LaCoO_3 (Fig. 2a). It is likely that specific surface area (SSA) is one of the important factors that is responsible for the difference between the relative sulfur uptake of Mn and Co-based perovskites. As we have reported in a previous publication, SSA for LaMnO_3 , Pd/LaMnO_3 , LaCoO_3 and Pd/LaCoO_3 are 20.6, 21.9, 7.1, and $8.9 \text{ m}^2 \text{ g}^{-1}$, respectively [33]. Thus, the higher SSA of Mn-based perovskites lead to a higher total SO_x uptake. As well as the surface area, relative surface basicity of perovskite materials also plays a significant role for SO_2 adsorption capabilities. It was stated in the literature that LaMnO_3 has a greater CO_2 adsorption capacity than that of LaCoO_3 , indicating a greater surface basicity of the former perovskite [26].

Thermal stability of SO_x species on LaCoO_3 and Pd/LaCoO_3 in vacuum are presented in the middle sets of spectra given in Fig. 2. SO_x species on both surfaces are stable on the catalyst surfaces up to 873 K. However, after annealing in vacuum at 1073 K, the Co-based perovskite samples reveal stark changes corresponding to the formation of bulk sulfates evident by the vibrational features located at 1166, 1102, and 1064 cm^{-1} [34]. Furthermore, distinctly sharp vibrational features corresponding to these bulk sulfate species may be associated with the formation of well-defined/ordered metal-sulfate domains such as $\text{La}_2(\text{SO}_4)_3$ on the LaCoO_3 and Pd/LaCoO_3 surfaces. This observation is consistent with a related work by Wang et al. who reported that on $\text{La}_{0.9}\text{Sr}_{0.1}\text{CoO}_3$, SO_2 led to the formation of $\text{La}_2(\text{SO}_4)_3$ on the surface and $\text{La}_2(\text{SO}_4)_3$, $\text{La}_2(\text{SO}_3)_3$, $\text{La}_2\text{O}_2\text{SO}_4$ and CoO , Co_3O_4 in the bulk [28, 38].

Regeneration of the sulfated LaCoO_3 and Pd/LaCoO_3 surfaces with H_2 is shown in the topmost sets of spectra given Fig. 2. While SO_x species on LaCoO_3 are mostly stable in H_2 up to 773 K, attenuation of SO_x vibrational features (located at 1248, 1185, 1138, 1054, and 986 cm^{-1}) are observed in the case of Pd/LaCoO_3 . Further reduction with H_2 at higher temperatures within 773–973 K gradually diminishes the SO_x IR intensities for both LaCoO_3 and Pd/LaCoO_3 , where SO_x species seem to almost disappear after reduction at 973 K. Unlike the Mn-based perovskites, where almost complete SO_x elimination was achieved at 873 K (upper sets of spectra in Fig. 1), LaCoO_3 and Pd/LaCoO_3 exhibit a relatively limited SO_x reduction capability in H_2 (upper sets of spectra in Fig. 2). This can also be attributed to the formation of cobalt sulfates and partial destruction of the perovskite structure after the poisoning process [31, 39].

Reduction of the Co-based perovskites with H_2 also reveals a very striking spectral alteration at elevated temperatures where the baselines of the IR spectra undergo a

significant modification and become oblique. Considering the fact that optical conditions in the spectroscopic setup as well as the positioning of the catalysts in the spectroscopic cell were invariant, this baseline deviation might be associated with electronic and structural aberrations in the LaCoO_3 and Pd/LaCoO_3 catalysts. It is likely that under these reducing conditions, the structural integrity of the Co-based perovskites was compromised, which may be associated with the reduction of the Co^{3+} (B-site) cations, partial destruction and phase segregation of the perovskite structure and formation of $\text{Co}^0/\text{CoO}/\text{La}_2\text{O}_3$ domains [25, 40–43]. This phenomenon has also been reported in one of our previous studies [33] where it was observed that interaction of Co-based perovskites with H_2 in the absence of SO_x species also led to the partial destruction of the perovskite structure and the reduction of Co^{3+} sites. This particularly mild reduction phenomenon is rather reversible, where exposing the partially reduced Co-based perovskites to air under ambient conditions allows the recovery of the perovskite structure as verified by XPS, XRD and Raman spectroscopic analysis (data not shown). Thus, it is likely that the mild and reversible reduction process taking place during the current experiments on the Co-based perovskites predominantly affects the surface/near-surface region of the catalysts without inflicting an irreversible bulk/deep reduction [41]. Furthermore, comparison of the extent of the baseline tilt upon reduction reveals a less prominent effect for Pd/LaCoO_3 compared to LaCoO_3 . This behavior has also been discussed in our former report [33], where we have demonstrated that Pd-supported perovskites has a favorable influence on the preservation of the structural stability of Co-based perovskites under reducing conditions. It should be noted that although Pd/LaCoO_3 was found to have the highest NO_x storage capacity among all other investigated perovskites [33], it has also a higher tendency for sulfur uptake.

3.3 Quantitative Surface Analysis via XPS

XPS analyses were performed in order to provide a semi-quantitative basis for the relative sulfur uptake of the investigated catalytic architectures. Figure 3 presents Mn/La and S/La relative surface atomic ratios that were evaluated from the integrated intensities of the $\text{Mn}2p$, $\text{La}3d_{5/2}$ and $\text{S}2p$ core level photoelectron spectra of the LaMnO_3 and Pd/LaMnO_3 samples after sulfation or after reduction of sulfates in $\text{H}_2(\text{g})$. Note that prior to the XPS measurements, samples were treated with significantly higher (i.e. fivefold greater) SO_x exposures as compared to that of the in situ FTIR experiments given in Figs. 1 and 2 in order to improve the signal to noise ratio (S/N) of the $\text{S}2p$ XP spectra. The insets in Fig. 3 present FTIR spectra of the same samples investigated in the XPS experiments which

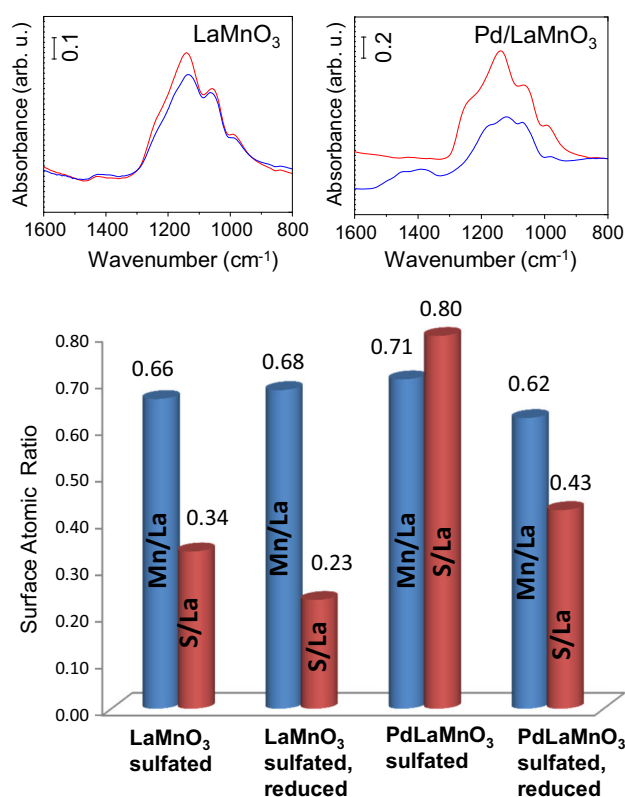


Fig. 3 Surface atomic ratios of sulfated (2.0 Torr, SO₂:O₂ = 1:10 at 673 K) and sulfated + reduced (under 2.0 Torr of H₂ for 15 min at 773 K) LaMnO₃ and Pd/LaMnO₃ samples via XPS (see text for details). Insets present the FTIR spectra of the same samples investigated in the XPS experiments, where red and blue spectra correspond to sulfated and sulfated + reduced samples; respectively

were exposed to high levels of SO_x. It should be noted that in all samples except Pd/LaMnO₃, which was sulfated and subsequently reduced, sulfur was found only in the form of SO₄²⁻ (i.e. S⁶⁺). On the surface of the reduced Pd/LaMnO₃ sample, along with sulfates, some sulfites and sulfides were also detected with a relative abundance of 100:10:15, respectively. The reduction of the sulfated LaMnO₃ sample leads to a significant decrease in the S/La ratio (i.e. by ~30 %). Based on the XPS data, Pd/LaMnO₃ seems to accumulate twice the amount of SO_x with respect to LaMnO₃. However, Pd/LaMnO₃ catalyst also seems to eliminate a greater fraction (ca. 45 %) of the adsorbed SO_x species upon reduction. These results are in good agreement with the corresponding FTIR spectra presented in the insets. The perovskite surfaces are enriched with lanthanum as was discussed in detail in one of former reports [33]. It is also worth mentioning that no appreciable changes in the surface Mn/La ratios were detected after sulfation and reduction of both LaMnO₃ and Pd/LaMnO₃ catalysts, reflecting the structural stability of these systems against sulfation and reduction with H₂.

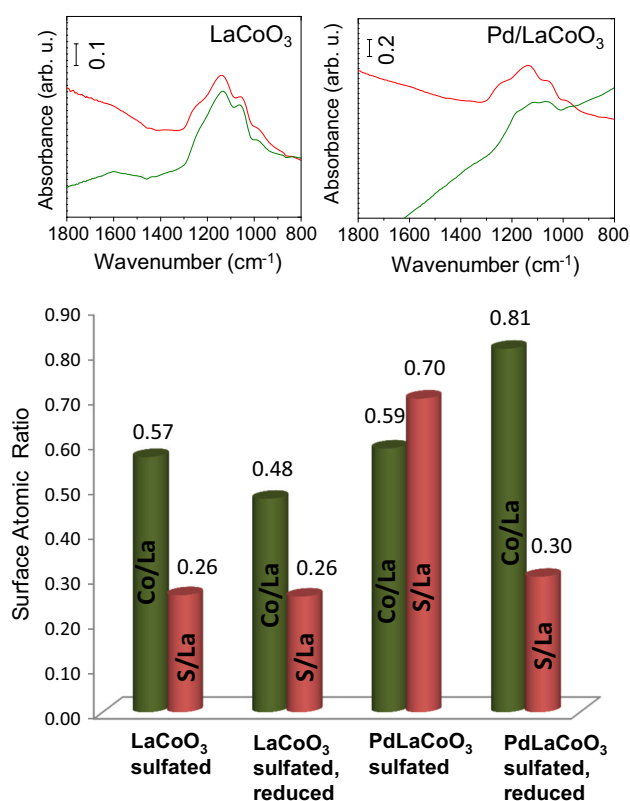


Fig. 4 Surface atomic ratios of sulfated (2.0 Torr, SO₂:O₂ = 1:10 at 673 K) and sulfated + reduced (under 2.0 Torr of H₂ for 15 min at 773 K) LaCoO₃ and Pd/LaCoO₃ samples via XPS (see text for details). Insets present the FTIR spectra of the same samples investigated in the XPS experiments, where red and green spectra correspond to sulfated and sulfated + reduced samples; respectively

Similar XPS analysis measurements were also carried out for Co-based perovskite catalysts (Fig. 4). For the sulfated LaCoO₃ and Pd/LaCoO₃ samples, sulfur was only found in the S⁶⁺ state (i.e. in the form of sulfates). On the other hand, for the sulfated and reduced Pd/LaCoO₃ sample, sulfite and sulfide species were also detected with relative SO₄²⁻:SO₃²⁻:S²⁻ abundances of 100:11:35, respectively. The sulfur content does not decrease significantly upon reduction of the sulfated LaCoO₃ sample. As in the case of Mn-based perovskites, Pd addition into the LaCoO₃ system favorably enhances the regeneration performance under hydrogen. This is evident by the strong decrease in the S/La ratio (ca. 55 %) of Pd/LaCoO₃ after reduction, in spite of the decrease in the relative abundance of La on the surface (i.e. attenuation of the Co/La ratio after reduction of the poisoned surface). Relatively strong alterations in the Co/La ratios of LaCoO₃ and Pd/LaCoO₃ surfaces upon reduction reflects the relative instability of these perovskites under reducing conditions which is in agreement with the baseline tilt observed in the corresponding FTIR spectra given in the insets of Fig. 4 [25, 40–43].

3.4 Preferential Adsorption Sites for SO_x (g)

An important aspect that is worth investigating is to determine whether SO_x species has any preference for particular adsorption sites on the Pd/LaMnO₃ and Pd/LaCoO₃ catalyst surfaces. In order to investigate this issue, CO was used as a probe molecule in the competitive sequential adsorption of SO_x and CO. Since CO can potentially adsorb on both Pd and perovskite sites, its co-adsorption/substitution with/by SO_x may yield some insight regarding poisoning of different adsorption sites on the catalyst surface. FTIR spectra recorded after CO saturation of the fresh and pre-sulfated (i.e. poisoned) Pd/LaMnO₃ surfaces are presented in Fig. 5. Adsorption of CO (50 Torr for 1 h at 323 K) on fresh surface (top spectrum) reveals a set of vibrational features at 2070, 1980, 1931, 1504, 1463, and 1346 cm⁻¹. While the first feature in spectrum (a) of Fig. 5 (i.e. 2070 cm⁻¹) corresponds to a-top coordination, the latter two features at 1980 and 1931 cm⁻¹ correspond to CO adsorbed on two and threefold coordination sites on metallic Pd, respectively [44–48]. It is important to mention that XPS analysis of the Pd/LaMnO₃ and Pd/LaCoO₃ samples reported in our former studies [33] indicates the presence of exclusively oxidized Pd states (i.e. Pd²⁺) after the catalyst synthesis, without any indication of metallic Pd surface sites. Thus, it is apparent that in the presence of excess CO (i.e. 50 Torr), PdO/PdO_x surface species are

reduced to metallic Pd⁰ species (Fig. 5). This argument is in very good agreement with previous observations reported in the literature, where Tessier et al. showed that surface PdO species can be readily reduced to metallic Pd in the presence of CO (g) at room temperature [49]. The lack of CO vibrational features within 2120–2110 and 2180–2160 cm⁻¹ in Fig. 5, which are associated with CO adsorbed on Pd⁺ and Pd²⁺ species [49], respectively; also indicates the absence of oxidized Pd surface sites on CO-saturated Pd/LaMnO₃ surface.

On the other hand, vibrational features in Fig. 5 at 1504, 1463, and 1346 cm⁻¹ can be attributed to carbonate species on the perovskite sites of the Pd/LaMnO₃ surface due to the presence of Lewis-basic surface sites [50–52]. Lack of oxidized Pd adsorption sites due to the reducing effect of CO also enables us to rule out the presence of carbonates on the Pd-containing domains to a great extent, suggesting that carbonates are likely to be formed mostly on the perovskite sites. An identical CO exposure was also introduced over the pre-sulfated (2.0 Torr of SO₂ + O₂ gas mixture, SO₂:O₂ = 1:10, 673 K, 30 min) Pd/LaMnO₃ surface (bottom spectrum in Fig. 5) at 323 K. Note that in this poisoning treatment, a high temperature of 673 K was employed, in order to ensure strong sulfation. No vibrational features related to CO adsorption was detected on the pre-sulfated Pd/LaMnO₃ surface indicating that both Pd and perovskite sites are poisoned simultaneously. FTIR

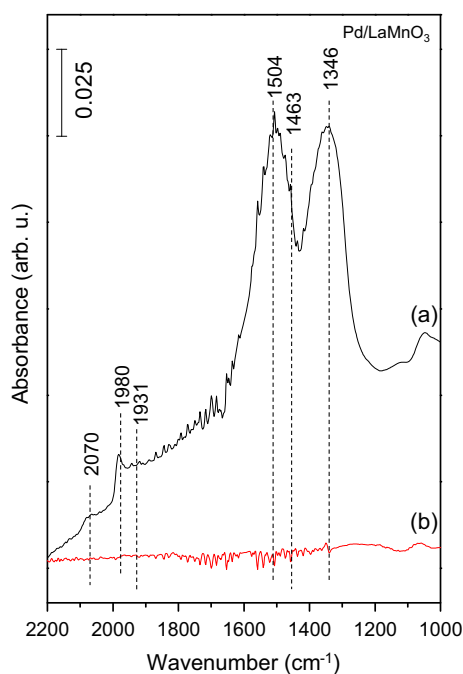


Fig. 5 FTIR spectra acquired after CO (g) adsorption [50.0 Torr of CO (g) for 1 h at 323 K] on *a* fresh Pd/LaMnO₃ and *b* pre-sulfated (2.0 Torr, SO₂:O₂ = 1:10, at 673 K) Pd/LaMnO₃. All spectra were acquired at 323 K in vacuum

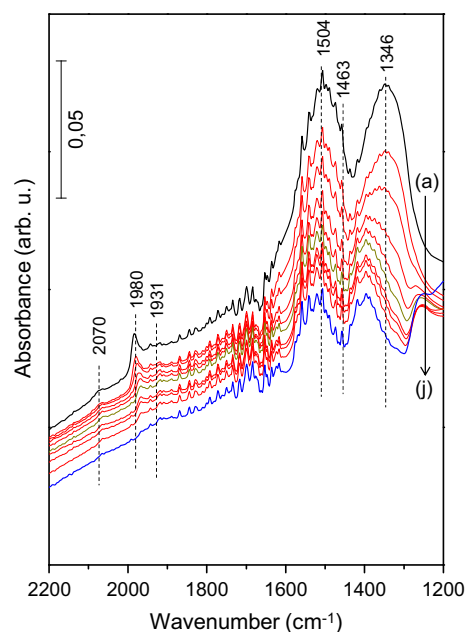


Fig. 6 FTIR spectra collected upon CO (g) adsorption [50.0 Torr of CO (g) for 1 h at 323 K] on *a* Pd/LaMnO₃. Set of IR spectra from *b* to *j* were recorded by SO_x (SO₂:O₂ = 1:10 at 323 K for 1 min) exposure with incremental pressure in between 0.1 and 2.0 torr. Finally, *j* corresponds to extreme SO_x (2.0 Torr, SO₂:O₂ = 1:10 at 323 K for 5 min) exposure. All spectra were acquired at 323 K in vacuum

data presented in Fig. 5 clearly demonstrate that under extreme poisoning conditions, adsorption sites on the Pd/LaMnO₃ catalyst surface are poisoned in a rather non-preferential manner.

Figure 6 illustrates the FTIR experiments where SO_x mixture (2.0 Torr of SO₂ + O₂ gas mixture (SO₂:O₂ = 1:10)) was gradually introduced over the CO pre-adsorbed (topmost black spectra) surface. In these set of experiments gradual displacement of the relatively weakly bound pre-adsorbed CO species with strongly bound SO_x species are apparent. Spectra in Fig. 6 suggest that SO_x species can readily substitute relatively weakly adsorbed carbonyl functionalities on the Pd sites [45, 53], while carbonate species formed on the perovskite sites reveal a stronger resistance against displacement due to their relatively higher adsorption energy [54]. In addition, these results also do not rule out the possibility that Pd sites can be relatively more prone to sulfur poisoning with respect to that of the perovskite adsorption sites during the initial stages of poisoning. Under regular operational regime of a DeNO_x catalyst, a significant amount of CO and CO₂ exists in the gas stream together with SO_x species. Thus, it is likely that carbonate functionalities located on the perovskite domains may direct the SO_x species towards the available Pd sites during the initial stages of poisoning. In other words, it is plausible that Pd sites may function as sacrificial sites at least during the initial stages of sulfur poisoning. Considering the operation of an NSR catalyst where the catalyst undergoes frequent switches between lean (i.e. oxidizing atmosphere where competitive NO_x/CO_x/SO_x uptake occurs) and rich (i.e. reducing atmosphere where NO_x/CO_x/SO_x reduction takes place) cycles; the catalyst is typically in a partially-poisoned state. Thus, the sulfur poisoning behavior of such catalytic systems may be predominantly governed by the initial stages of SO_x uptake as described above.

It is worth mentioning that similar competitive CO/SO_x adsorption experiments were also carried out on the Pd/LaCoO₃ catalyst. However since this surface is opaque to the transmission of IR radiation above 1700 cm⁻¹, (i.e. the IR spectral region where the metal carbonyl features are located), no comparable data was obtained in these experiments. However, based on the similarities in the NO_x [33] and SO_x adsorption properties of Pd/LaMnO₃ and Pd/LaCoO₃ surfaces, we anticipate a similar interplay between CO and SO_x on Pd/LaCoO₃ as in the case of Pd/LaMnO₃.

3.5 Effect of S-poisoning on the NO_x Adsorption Capacity of Perovskites

Figure 7 illustrates FTIR spectra taken after NO_x saturation of fresh and sulfated LaMnO₃ and Pd/LaMnO₃ samples. The black spectra correspond to NO_x adsorption on fresh

material and red spectra correspond to NO_x adsorption on pre-sulfated material surface. Assignment of the nitrate/nitrite absorption features on fresh perovskite surfaces was discussed comprehensively in one of our former reports [33]. Briefly, IR features located at around 1649 and 1009 cm⁻¹ can be assigned to asymmetric and symmetric stretching modes of bridging nitrate species on the perovskite surfaces, respectively [55]. Features located at 1530 and 1269 cm⁻¹ can be attributed to stretching vibrations of monodentate nitrates. The IR features at 1568 and 1246 cm⁻¹ correspond to bidentate nitrates [56, 57]. The set of characteristic features observed at 1487, 1430, 1321, and 839 cm⁻¹ can be ascribed to nitrito species on the perovskite surface [58–61]. It should be noted that NO_x species (i.e. nitrites and nitrates) residing on Pd sites are difficult to discern from the NO_x species adsorbed on the perovskite domains due to the relatively low loading of Pd present in the catalyst formulation as well as the overlapping vibrational frequencies. Thus, the competitive adsorption trends observed for the data presented in Figs. 6 is not trivially visible in the data presented in Figs. 7 and 8.

It is obvious that pre-sulfation leads to suppression of nitrate/nitrite related features of NO_x saturated LaMnO₃ and Pd/LaMnO₃ samples demonstrating competition between SO_x and NO₂ for the same adsorption sites (Fig. 7). Suppression of the nitrate/nitrite features upon NO₂ adsorption after sulfur poisoning can be readily explained by the occupation of some of the NO_x adsorption sites by the thermodynamically more stable surface sulfate species and formation of species such as La₂(SO₄)₃ [28, 38, 62]. In Fig. 7a, relative vibrational intensity of 1322 cm⁻¹ (nitrite species) diminishes more visibly as compared to the feature at 1263 cm⁻¹ (monodentate nitrates) after sulfur poisoning. Similarly, on Pd/LaMnO₃ (Fig. 7b), attenuation in the relative vibrational intensity of 1328 cm⁻¹ (nitrite species) is more pronounced as compared to that of 1279 cm⁻¹ (monodentate nitrates) upon sulfur poisoning. This behavior reveals that monodentate geometry of surface nitrates becomes more preferable after sulfation of the surfaces probably due to the limited number of available perovskite adsorption sites on the poisoned materials.

As already demonstrated in our previous report [33], the total NO₂ adsorption capacity of fresh LaMnO₃ and Pd/LaMnO₃ are comparable to each other. However, after sulfur poisoning, Pd/LaMnO₃ accumulates less NO₂. Figure 7a indicates that the IR bands associated with the NO_x species on the Pd-free LaMnO₃ sample have a moderate attenuation upon S-poisoning. On the other hand, the Pd/LaMnO₃ sample (Fig. 7b) reveals a stronger attenuation. This is in perfect agreement with the results presented in previous sections suggesting that Pd-supported perovskite materials leads to higher SO_x accumulation/adsorption on the surface.

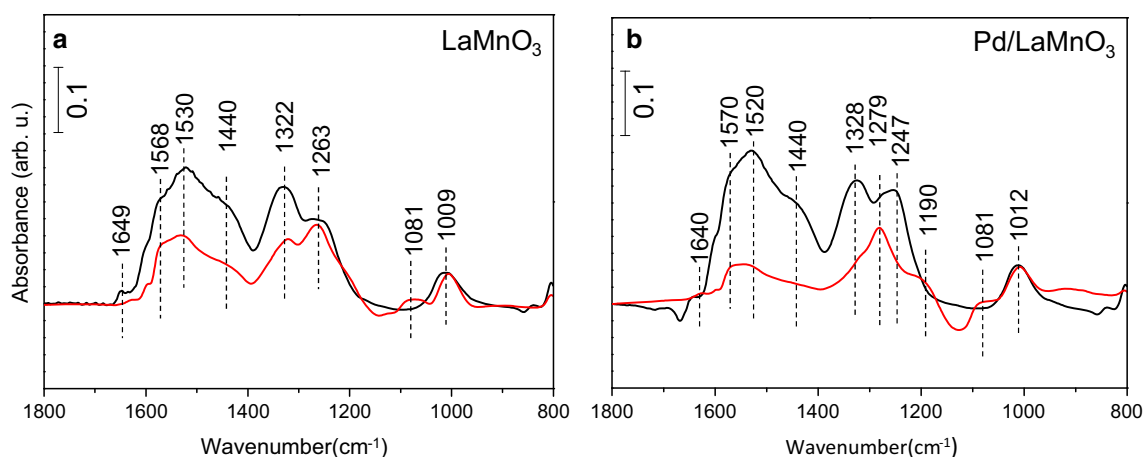


Fig. 7 FTIR spectra acquired after NO₂ saturation [5.0 Torr NO₂ (g), 323 K, 10 min] of fresh (*black* spectra) and S-poisoned surfaces (*red* spectra) via 2.0 Torr, 673 K, SO₂:O₂ = 1:10. **a** LaMnO₃ and **b** Pd/

LaMnO₃. All spectra were acquired at 323 K in vacuum. Note that the background FTIR spectra for the *red* curves were obtained after sulfur poisoning and before NO₂ adsorption

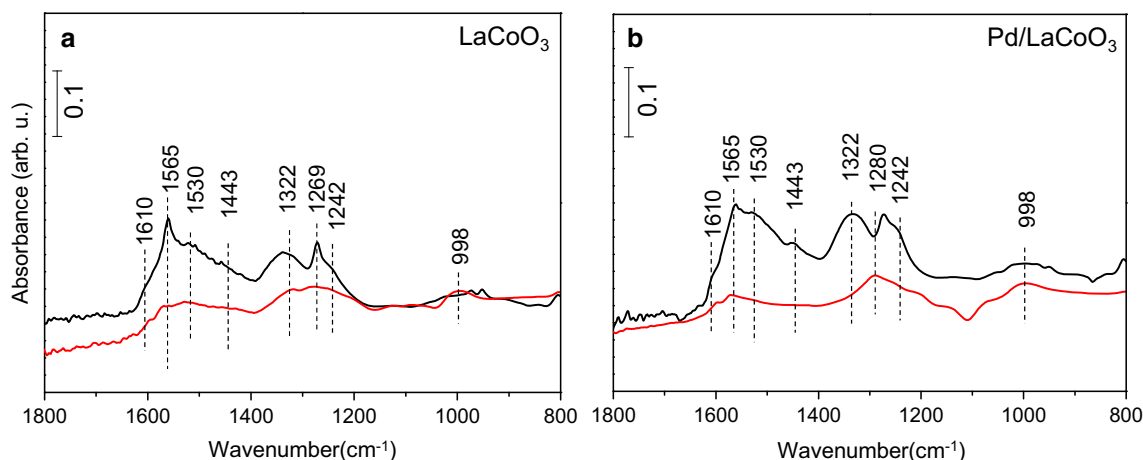


Fig. 8 FTIR spectra acquired after NO₂ saturation [5.0 Torr NO₂ (g), 323 K, 10 min] of fresh (*black* spectra) and S-poisoned surfaces (*red* spectra) via 2.0 Torr, 673 K, SO₂:O₂ = 1:10. **a** LaCoO₃ and **b** Pd/

LaCoO₃. All spectra were acquired at 323 K in vacuum. Note that the background FTIR spectra for the *red* curves were obtained after sulfur poisoning and before NO₂ adsorption

An identical set of experiments was also performed for the LaCoO₃ and Pd/LaCoO₃ materials (Fig. 8). After sulfation, the 1322 cm⁻¹ (nitrito species) and 1242 cm⁻¹ (bidentate nitrates) bands are suppressed while the band at 1293 cm⁻¹ (monodentate nitrates) still persists. Thus, as in the case of Mn-based perovskite systems, Co-based perovskites also lose their NO_x storage capacity significantly upon SO_x poisoning with the formation of lanthanum and cobalt sulfate species [28, 31, 38, 39].

3.6 Sulfur Regeneration Under Vacuum via TPD Analysis

TPD experiments were carried out in order to examine the thermal regeneration characteristics as well as the relative adsorption strengths of adsorbed sulfur species on each synthesized perovskite material in the absence of an

external reducing agent. Only O₂, H₂S, and SO₂ desorption channels (corresponding to mass to charge ratios of $m/z = 32$, 34, and 64; respectively) revealed significant QMS signals during the TPD experiments. Note that since the contribution of SO₂ and H₂S to the $m/z = 32$ desorption signal is relatively minor. Thus, $m/z = 32$ desorption channel can be predominantly attributed to O₂ desorption. Figure 9 presents the TPD profiles for $m/z = 32$ and 64 (i.e. O₂ and SO₂ desorption channels; respectively) regarding the thermal decomposition of pre-adsorbed sulfate and sulfite species on (a) LaMnO₃, (b) Pd/LaMnO₃, (c) LaCoO₃, and (d) Pd/LaCoO₃ surfaces; respectively. Sulfur-related species revealed high thermal stability for all of the synthesized materials which is evident by the lack of any desorption/decomposition signals at $T < 850$ K. Analysis of the similar line shapes for the O₂ and SO₂ traces revealing similar intensities and similar thermal

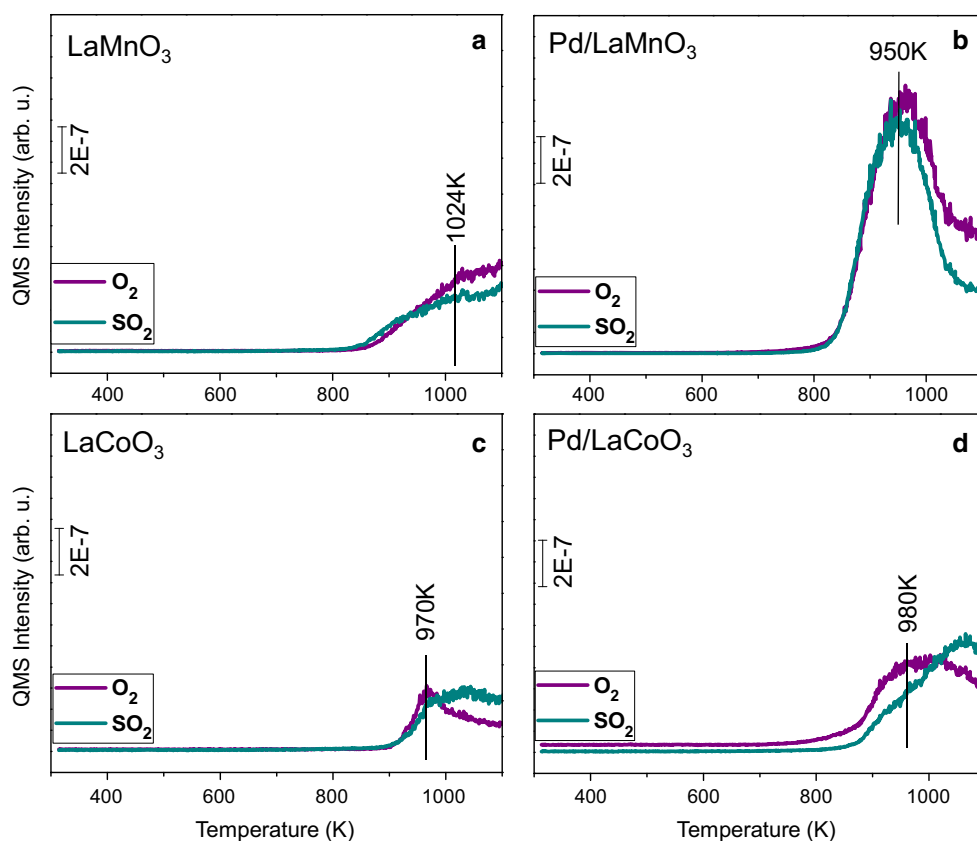


Fig. 9 TPD profiles for **a** LaMnO₃, **b** Pd/LaMnO₃, **c** LaCoO₃ and **d** Pd/LaCoO₃ after 2.0 Torr SO_x (2 Torr SO₂ + O₂, SO₂:O₂ = 1:10) adsorption at 673 K for 30 min

dependences in Fig. 9a suggests that within the thermal window investigated in the TPD experiments (i.e. 323–1073 K), sulfates desorb in the form of SO₂ (g) + O₂ (g) from the LaMnO₃ surface. It is also apparent in Fig. 9a that the maximum temperature that can be attained in the current TPD setup (i.e. 1073 K) is not sufficient to remove most of the SO_x species from the LaMnO₃ surface evident by the monotonically increasing desorption signals with increasing temperature without any desorption maxima. In other words, thermal SO_x desorption maximum of LaMnO₃ is located at $T > 1073$ K. This is in perfect agreement with the in situ FTIR spectra presented in the middle section of Fig. 1a, corresponding to experiments reflecting similar conditions. On the other hand, SO_x-TPD data for the Pd/LaMnO₃ (Fig. 9b) indicates noticeable dissimilarities both in terms of relative desorption temperatures and desorption intensities as compared to that of Fig. 9a. For Pd/LaMnO₃, $m/z = 32$ and $m/z = 64$ desorption channels reveal intense temperature maxima at ca. 950 K. It is apparent that the presence of Pd sites noticeably facilitates the thermal decomposition of SO_x species in the form of SO₂ (g) + O₂ (g). This observation is in very good agreement with the in situ FTIR data given in the middle section of Fig. 1b at 1073 K, representing conditions that are comparable to the

ones corresponding to the completion of the TPD experiments.

Figure 9c, d show similar SO_x-TPD experiments for LaCoO₃ and Pd/LaCoO₃ catalysts; respectively. The most prominent feature of these TPD data are the relatively weak desorption maxima located at ca. 970–980 K suggesting the simultaneous evolution of SO₂ (g) + O₂ (g). However, unlike the data in Fig. 9a, b, TPD data given in Fig. 9c, d also present a shoulder at $T > 1000$ K where O₂ (g) desorption intensity exceeds that of the SO₂ (g) signal. This observation suggests that at elevated temperatures, it is likely that in addition to the thermal decomposition of sulfates [SO₄²⁻(ads, bulk)], cobalt-based perovskites also undergo thermal reduction at elevated temperatures leading to the formation of oxygen vacancies, partial destruction of the perovskite lattice and the formation of thermally-stable new species such as La₂(SO₄)₃, La₂(SO₃)₃, CoSO₄, CoSO₃, Co₂(SO₃)₃, and Co₂(SO₄)₃. This argument is in line with the formation of sharp and intense vibrational features for the 1073 K spectra in the middle section of the Fig. 2a, b.

Figure 10 shows the $m/z = 34$ desorption channel corresponding to H₂S (g) evolution which is acquired simultaneously with the set of TPD spectra given in Fig. 9. It is

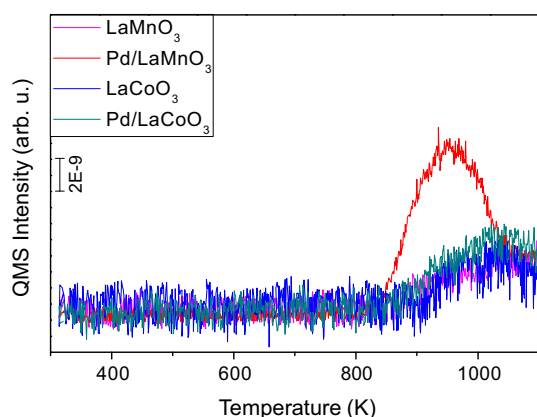


Fig. 10 H_2S desorption profiles for LaMnO_3 , Pd/LaMnO_3 , LaCoO_3 and Pd/LaCoO_3 after 2.0 Torr SO_x (2 Torr $\text{SO}_2 + \text{O}_2$, $\text{SO}_2:\text{O}_2 = 1:10$) adsorption at 673 K for 30 min

apparent in Fig. 10 that within the investigated thermal window, H_2S evolution is relatively limited for all samples except for Pd/LaMnO_3 . This can possibly be attributed to two factors. Firstly, the SSA of Pd/LaMnO_3 is almost three times greater than that of the LaCoO_3 and Pd/LaCoO_3 catalysts. Thus, on the Pd/LaMnO_3 catalyst, the presence of -OH minority species might be more pronounced than the cobalt-based samples, allowing the observation of a more significant H_2S (g) desorption signal. Secondly, it is also probable that H_2S (g) desorption process is catalyzed by the surface Pd sites, as it is not observed on the LaMnO_3 surface which lacks any Pd species.

4 Conclusions

In the current work, LaMnO_3 , Pd/LaMnO_3 , LaCoO_3 and Pd/LaCoO_3 perovskite catalysts were synthesized and their structural as well as sulfur poisoning properties were thoroughly studied by means of in situ FTIR spectroscopy, XPS, and TPD. Our findings can be summarized as follows:

- SO_x adsorption capacity of LaMnO_3 (per mass of catalyst) is greater than that of LaCoO_3 . This can tentatively be attributed to the significantly higher specific surface area.
- SO_x adsorption capacity significantly increases in the presence of Pd for both Mn- and Co-based perovskites.
- On Co-based perovskite systems, surface sulfates transform (at least partially) into stable bulk sulfate species at $T \geq 1073$ K in the absence of a reducing agent.
- Sulfates on LaMnO_3 and LaCoO_3 are resilient against reduction by H_2 and can be eliminated only at elevated temperatures (i.e. $T > 873$ K) under reducing

conditions. On the other hand, sulfates on Pd-containing perovskites can be reduced at lower temperatures such as 773 K in the presence of H_2 .

- Competitive CO and SO_x adsorption experiments suggest that Pd sites reveal a greater tendency towards SO_x species particularly in the early stages of sulfur poisoning as compared to the perovskite surface sites. Thus, Pd sites may function as sacrificial SO_x storage sites in the early stages of sulfur poisoning.
- SO_x species significantly attenuate the NO_2 and CO adsorption capacities. However, even after severe SO_x poisoning, NO_x adsorption on perovskite systems can still continue to occur in the form of monodentate nitrates and nitrites.
- Even if Co-containing perovskites have higher NO_x storage capacity, Mn-based perovskites have higher stability against H_2 and are more resilient against sulfur poisoning rendering the latter catalysts promising for NSR applications.

Acknowledgments The authors acknowledge the financial support from the Scientific and Technical Research Council of Turkey (TUBITAK) (Project Code: 213M585 and TUBITAK 2221 Fellowship Program). Authors also acknowledge the scientific collaboration with TARLA project founded by the Ministry of Development of Turkey under grant no DPT2006K-120470.

References

1. Epling WS, Campbell LE, Yezerets A, Currier NW, Parks JE (2004) *Catal Rev* 46:163–245
2. Matsumoto S (2000) *Cattech* 4:102–109
3. Roy S, Baiker A (2009) *Chem Rev* 109:4054–4091
4. Kato K, Nohira H, Nakanishi K, Iguchi S, Kihara T, Muraki H (1993) *Euro Patent Application* 0,573,672 A1
5. Miyoshi N, Matsumoto S, Katoh K, Tanaka T, Harada K, Takahashi N, Yokota K, Sugiura M, Kasahara K (1995) *SAE Technical Papers Series No.* 950809
6. Takahashi N, Shinjoh H, Iijima T, Suzuki T, Yamazaki K, Yokota K, Suzuki H, Miyoshi N, Matsumoto S, Tanizawa T, Tanaka T, Tateishi S, Kasahara K (1996) *Catal Today* 27:63–69
7. Ozensoy E, Peden CHF, Szanyi J (2006) *J Catal* 243:149–157
8. Andonova SM, Senturk GS, Kayhan E, Ozensoy E (2009) *J Phys Chem C* 113:11014–11026
9. Kayhan E, Andonova SM, Senturk GS, Chusuei CC, Ozensoy E (2009) *J Phys Chem C* 114:357–369
10. Andonova SM, Senturk GS, Ozensoy E (2010) *J Phys Chem C* 114:17003–17016
11. Emmez E, Vovk EI, Bukhtiyarov VI, Ozensoy E (2011) *J Phys Chem C* 115:22438–22443
12. Vovk EI, Emmez E, Erbudak M, Bukhtiyarov VI, Ozensoy E (2011) *J Phys Chem C* 115:24256–24266
13. Senturk GS, Vovk EI, Zaikovskii VI, Say Z, Soylu AM, Bukhtiyarov VI, Ozensoy E (2012) *Catal Today* 184:54–71
14. Hummatov R, Gulseren O, Ozensoy E, Toffoli D, Ustunel H (2012) *J Phys Chem C* 116:6191–6199
15. Say Z, Vovk EI, Bukhtiyarov VI, Ozensoy E (2013) *Top Catal* 56:950–957

16. Vovk EI, Turksoy A, Bukhtiyarov VI, Ozensoy E (2013) *J Phys Chem C* 117:7713–7720
17. Say Z, Vovk EI, Bukhtiyarov VI, Ozensoy E (2013) *Appl Catal B* 142–143:89–100
18. Say Z, Tohumeken M, Ozensoy E (2014) *Catal Today* 231:135–144
19. Kröcher O, Elsener M (2008) *Appl Catal B* 77:215–227
20. Andonova S, Vovk EI, Sjöblom J, Ozensoy E, Olsson L (2014) *Appl Catal B* 147:251–263
21. Kim CH, Qi G, Dahlberg K, Li W (2010) *Science* 327:1624–1627
22. Rousseau S, Lorient S, Delichere P, Boreave A, Deloume J, Vernoux P (2009) *Appl Catal B* 88:438–447
23. Li N, Boreave A, Deloume J, Gaillard F (2008) *Solid State Ion* 179:1396–1400
24. Royer S, Duprez D, Can F, Courtois X, Dupeyrat CB, Laassiri S, Alamdari H (2014) *Chem Rev* 114(20):10292–10368
25. Peña MA, Fierro JL (2001) *Chem Rev* 101:1981–2018
26. Rossetti I, Buchneva O, Biffi C, Rizza R (2009) *Appl Catal B* 89:383–390
27. Li X, Chen C, Liu C, Xian H, Guo L, Lv J, Jiang Z, Vernoux P (2013) *ACS Catal* 3:1071–1075
28. Zhu Y, Tan R, Feng J, Ji S, Cao L (2001) *Appl Catal A* 209:71–77
29. Zhang R, Alamdari H (2008) *Kaliaguine. S Appl Catal A* 340:140–151
30. Koponen MJ, Venalainen T, Suvanto M, Kallinen K, Kinnunen TJJ, Harkonen M, Pakkanen TA (2006) *J Mol Catal A* 258:246–250
31. Wang X, Qi X, Chen Z, Jiang L, Wang R, Wei K (2014) *J Phys Chem C* 118:13743–13751
32. Kim CH, Li W, Dahlberg KA US Patent 7, 964, 167 B2
33. Say Z, Dogac M, Vovk EI, Kalay YE, Kim CH, Li W, Ozensoy E (2014) *Appl Catal B* 154–155:51–61
34. Rosso I, Garrone E, Geobaldo F, Onida B, Saracco G, Specchia V (2001) *Appl Catal B* 34:29–41
35. Hoffman FM (1983) *Surf Sci Rep* 3:107–192
36. Waqif M, Bazin P, Saur O, Lavalley JC, Blanchard G, Touret O (1997) *Appl Catal B* 11:193–205
37. Furfori S, Russo N, Fino D, Saracco G, Specchia V (2010) *Chem Eng Sci* 65:120–127
38. Wang H, Zhu Y, Tan R, Yao W (2002) *Catal Lett* 82:199–204
39. Ammendola P, Cammisa E, Chirone R, Lisi L, Ruoppolo G (2012) *Appl Catal B* 113–114:11–18
40. Hung L, Bassir M, Kaliaguine S (2005) *Appl Surf Sci* 24:360–375
41. Crespin M, Hall WK (1981) *J Catal* 69:359–370
42. Dacquín JP, Dujardin C, Granger P (2008) *J Catal* 253:37–49
43. Bernard C, Durand B, Verelst M, Lecante P (2004) *J Mater Sci* 39:2821–2826
44. Ozensoy E, Min BK, Goodman DW (2004) *J Phys Chem B* 108:4351–4357
45. Szanyi J, Kuhn WK, Goodman DW (1993) *J Vac Sci Tech* 11:1969
46. Ozensoy E, Meier DC, Goodman DW (2002) *J Phys Chem B* 106:9367–9371
47. Ozensoy E, Goodman DW (2004) *Phys Chem Chem Phys* 6:3765–3778
48. Ozensoy E, Szanyi J, Peden CHF (2005) *J Phys Chem B* 109:3431–3436
49. Tessier D, Rakai A, Bozon-Verduraz F (1992) *J Chem Soc Faraday Trans* 88:741–749
50. Busca G, Lorenzelli V (1982) *Mater Chem* 7:89–126
51. Klingenberg B, Vannice MA (1996) *Chem Mater* 8:2755–2768
52. Mawdsley JR, Krause TR (2008) *Appl Catal A* 334:311–320
53. Haruta M, Yamada N, Kobayashi T, Iijima S (1989) *J Catal* 115:301–309
54. Patrito EM, Olivera PP (1998) *Electrochim Acta* 44:1237–1245
55. López-Suárez FE, Illán-Gómez MJ, Bueno-López A, Anderson JA (2011) *Appl Catal B* 104:261–267
56. Klingenberg B, Vannice MA (1999) *Appl Catal B* 21:19–33
57. Martínez-Arias A, Soria J, Conesa JC, Seoane XL, Arcoya A, Cataluna R (1995) *J Chem Soc Faraday Trans* 91:1679–1687
58. Hadjiivanov KI (2000) *Catal Rev Sci Eng* 42:71–144
59. Prinetto F, Ghiotti G, Nova I, Lietti L, Tronconi E, Forzatti P (2001) *J Phys Chem B* 105:12732–12745
60. Ghiotti G, Chiorino A (1993) *Spectrochim Acta A* 49:1345–1359
61. Low MJD, Yang RT (1974) *J Catal* 34:479–489
62. Elbouazzaoui S, Corbos EC, Courtois X, Marecot P, Duprez D (2005) *Appl Catal B* 61:236–243